

## OPERATING CAPACITY

The operating capacity of Auchlite A 102 D is obtained by multiplying the basic capacity value from Table 6 by the correction factor D to G from Tables 7 to 10.

$$\text{Cap} = \text{Cap}_0 \times D \times E \times F \times G$$

**TABLE 6 : Basic Capacity versus NaOH regenerant level ( counter current regeneration )**

NaOH g/L	Capacity eq/L ( Cap <sub>0</sub> )
30	0.65
40	0.82
50	0.92
60	0.98
70	1.04
80	1.06

**TABLE 7 : Capacity Correction Factor D versus Sulphate to Total Anions Ratio.**

SO <sub>4</sub> %	Factor D
0	0.94
25	0.97
50	1.00
75	1.03
99	1.06

**TABLE 8 : Capacity Correction Factor E versus Carbon Dioxide to Total Anions Ratio.**

CO <sub>2</sub> %	Factor E
0	0.97
20	1.00
30	1.02
50	1.05
75	1.08
99	1.12

**TABLE 9 : Capacity Correction Factor F versus Silica to Total Anions Ratio and NaOH Temperature(°C)**

	5	10	20	30% SiO <sub>2</sub>
5°C	0.96	0.93	0.87	0.83
10	0.97	0.94	0.89	0.85
15	0.98	0.95	0.91	0.87
20	0.99	0.96	0.92	0.89
25	1.00	0.98	0.94	0.90
30	1.01	0.99	0.93	0.92

**TABLE 10 : Capacity Correction Factor G versus Silica Endpoint (DSiO<sub>2</sub> = difference between average leakage and endpoint )**

DSiO <sub>2</sub> ( ppb )	Factor G
50	0.90
100	0.95
200	1.00
300	1.04

### SAFE USE INFORMATION

A Material Safety Data Sheet is available for each product. To obtain a copy contact your Auchtel representative.

### CAUTION

Acid and basic regenerant solutions are corrosive and should be handled in a manner that will prevent eye and skin contact. Nitric acid and other strong oxidizing agents can cause explosive type reactions when mixed with Ion Exchange Resins. Proper design of process equipment to prevent rapid buildup of pressure is necessary if use of an oxidizing agent, such as nitric acid is contemplated. Before using strong oxidizing agents in contact with Ion Exchange Resins, consult sources knowledgeable in the handling of these materials.

*The suggestions and data in this bulletin are based on information we believe to be reliable. They are offered in good faith, but without guarantee, as conditions and methods of use of our products are beyond our control. We recommend that the prospective user determine the suitability of our materials and suggestions before adopting them on a commercial scale. The Company maintains a policy of continuous development and reserve the right to amend any specification without notice.*

**Auchtel Products Ltd., 142 C, Victor House, N.M. Joshi Marg, Lower Parel(w), Mumbai-400 013**

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# SEPARATION TECHNOLOGIES

## ION EXCHANGE RESINS

# AUCLITE A 102 D

## ENGINEERING DATA SHEET (COUNTER CURRENT REGENERATION)



Auchlite A 102 D is a type 2 strong base Anion Exchange Resin. These data provide information to calculate the silica leakage and operating capacity of Auchlite A 102 D used with counter current regeneration.

The properties of Auchlite A 102 D are described in the product Data Sheet.

### SILICA LEAKAGE

The average silica leakage is obtained by multiplying the basic leakage value from Table 1 by the correction factors A, B and C from Tables 2 to 4

$$LEAK = LEAK_0 \times A \times B \times C$$

**TABLE 1 : Basic Silica Leakage versus NaOH regenerant level.**

NaOH g / L	Leakage ppm SiO <sub>2</sub> (Leak <sub>0</sub> )
30	0.050
40	0.036
50	0.024
60	0.017
80	0.010

**TABLE 2 : Leakage Correction Factor A versus Silica to Total Anions Ratio.**

SiO <sub>2</sub> %	Factor A
1	0.2
5	0.5
10	1.0
20	2.0
30	3.0

**TABLE 3 : Leakage Correction Factor B versus Water Temperature..**

Water °C	Factor B
5	0.7
10	0.8
15	1.0
20	1.2
25	1.5
30	2.2

**TABLE 4 : Leakage Correction Factor C versus Regenerant Temperature.**

Water °C	Factor C
10	1.65
15	1.37
20	1.16
25	1.00
30	0.87

**TABLE 3 : Suggested Operating Conditions**

Maximum operating temperature.....	35 °C ( OH <sup>-</sup> ), 70 °C ( Cl <sup>-</sup> )
Minimum bed depth .....	1000 mm ( preferably > 1400 mm)
Service flow rate .....	5 to 40 BV* / h
Maximum linear velocity .....	40 m / h
Regenerant .....	NaOH
Level .....	30 to 70 g / L
Flow rate .....	2 to 8 BV/h ( minimum contact time : 30 minutes)
Concentration .....	3% to 5% .
Slow rinse .....	2 BV at regeneration flow rate
Fast rinse .....	2 to 12 BV at service flow rate.

\* 1 BV ( Bed Volume ) = 1 m<sup>3</sup> solution pe

# SEPARATION TECHNOLOGIES

## ION EXCHANGE RESINS

# AUCLITE A 102 D

## ENGINEERING DATA SHEET (CO-CURRENT REGENERATION)



Auchlite A 102 D is a type 2 strong base Anion Exchange Resin. These data provide information to calculate the silica leakage and operating capacity of Auchlite A 102 D used with co-current regeneration.

The properties of Auchlite A 102 D are described in the product Data Sheet.

### SILICA LEAKAGE

The average silica leakage is obtained by multiplying the basic leakage value from Table 1 by the correction factors A, B and C from Tables 2 to 4

$$LEAK = LEAK_0 \times A \times B \times C$$

**TABLE 1 : Basic Silica Leakage versus NaOH regenerant level.**

NaOH g / L	Leakage ppm SiO <sub>2</sub> ( Leak <sub>0</sub> )
50	0.120
60	0.081
80	0.039
100	0.028

**TABLE 2 : Leakage Correction Factor A versus Silica to Total Anions Ratio.**

SiO <sub>2</sub> %	Factor A
1	0.2
5	1.0
10	2.0
20	4.0
30	6.0

**TABLE 3 : Leakage Correction Factor B versus Water Temperature**

Water °C	Factor B
5	0.7
10	0.8
15	1.0
20	1.2
25	1.5
30	2.2

**TABLE 4 : Leakage Correction Factor C versus Regenerant Temperature**

Water °C	Factor B
10	1.65
15	1.70
20	1.16
25	1.00
30	0.87

**TABLE 3 : Suggested Operating Conditions**

Maximum operating temperature.....	35 °C ( OH <sup>-</sup> ), 70 °C ( Cl <sup>-</sup> )
Minimum bed depth .....	700 mm
Service flow rate .....	5 to 40 BV* / h
Maximum linear velocity .....	40 m / h
Regenerant .....	NaOH
Level .....	50 to 100 g / L
Flow rate .....	2 to 8 BV/ h ( minimum contact time : 30 minutes)
Concentration .....	3% to 5% .
Slow rinse .....	2 BV at regeneration flow rate
Fast rinse .....	2 to 12 BV at service flow rate.

\* 1 BV ( Bed Volume ) = 1 m<sup>3</sup> solution per

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The operating capacity of Auchlite A 102 D is obtained by multiplying the basic capacity value from Table 6 by the correction factor D to G from Tables 7 to 10.

$$\text{Cap} = \text{Cap}_0 \times \text{D} \times \text{E} \times \text{F} \times \text{G}$$

**TABLE 6 : Basic Capacity versus NaOH regenerant level ( Co-flow regeneration )**

NaOH g/L	Capacity eq/L ( Cap <sub>0</sub> )
50	0.85
60	0.91
70	0.96
80	0.99
100	1.03

**TABLE 7 : Capacity Correction Factor D versus Sulphate to Total Anions Ratio.**

SO <sub>4</sub> %	Factor D
0	0.94
25	0.97
50	1.00
75	1.03
99	1.06

**TABLE 8 : Capacity Correction Factor E versus CO<sub>2</sub> content ( % of Total Anions )**

CO <sub>2</sub> %	Factor E
0	0.97
20	1.00
30	1.02
50	1.05
75	1.08
99	1.12

**TABLE 9 : Capacity Correction Factor F versus Silica to Total Anions Ratio and NaOH Temperature(°C)**

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15	0.98	0.95	0.91	0.87
20	0.99	0.96	0.92	0.89
25	1.00	0.98	0.94	0.90
30	1.01	0.99	0.93	0.92

**TABLE 10 : Capacity Correction Factor G versus Silica Endpoint (DSiO<sub>2</sub> = difference between average leakage and endpoint )**

DSiO <sub>2</sub> ( ppb )	Factor G
50	0.90
100	0.95
200	1.00
300	1.04

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